

Synthetic Rutile – not just Fe Reduction



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Synthetic Rutile



- What is it?
- What is it for?
- Process outline
- Pigment industry

- Sulphate process
- TiO₂ solubility
- Reaction pathways
- M₃O₅ Crystal Form



What is SR and what is it used for?



- SR = high grade TiO₂ made from ilmenite (FeO.TiO₂)
 - Fe extraction from Ilmenite
 - Becher Process
 - exclusively in Western Australia.
 - 5 plants
 - ~14Mt of SR
- Hardware based on DRI technology
 - higher temperature 1100-1140°C



What is the process?



- Fe metallisation of ilmenite + hydrometallurgical extraction of the Fe(m)
 - Results in a porous TiO₂ grain:

Ilmenite FeO.TiO₂ +
$$(1+x)$$
CO(g) \rightarrow Fe(m) + TiO_{2-x} + $(1+x)$ CO₂(g)

Ilmenite – solid solution series of ferrotitanates e.g.

Pseudorutile
$$Fe_2O_3.3TiO_2 + CO(g) \rightarrow 2FeO.TiO_2 + TiO_2 + CO_2(g)$$

- Pseudorutile preferred:
 - more porous and thus more amenable to the Fe extraction process (the hydrometallurgy stage).
- Minerals are never pure!

STREET BESTERNES

- Mixture of ilmenite and altered ilmenites
- other elements Mn, Mg, Al, Cr, V

Mineralogy



The reduction process is not clear cut

- TiO₂ is partly reduced
 - TiO₂ to Ti₃O₅ (anosovite) and Ti₂O₃.
- Trace elements present
 - $-M_3O_5$ and M_2O_3 forms.
- Chloride pigment process
 - chlorination at 1000°C to form metal chlorides
 - mineralogy of the TiO₂ mineral irrelevant
- M₃O₅ (Pseudobrookite) avoided
 - trace elements are locked in it
 - = lower TiO₂ grade in SR.
- HTPS 2015 Dr Ian Grey CSIRO Key Note presentation
 - high levels of MgO in Victorian ilmenite ≠ SR production
 - H₂ based process to overcome this

Pigment Industry



- Two pigment processes
 - Chloride process

$$TiO_2 + 2Cl_2(g) + C = TiCl_4(g) + CO_2(g)$$
 900-1000°C
 $TiCl_4(g) + O_2(g) = TiO_2 + 2Cl_2(g)$

Sulphate process

FeO.TiO₂ +
$$2H_2SO_4$$
 = TiOSO₄ + FeSO₄ + $2H_2O$ 190-230°C
TiOSO₄ + H_2O = TiO(OH)₂ + H_2SO_4
TiO(OH)₂ = TiO₂ + H_2O (g) 900-1000°C

- Market Share ~50:50
- SR only addresses half the market



What is the Sulphate Process?



Digestion of mineral with concentrated sulphuric acid –

$$FeO.TiO_2 + H_2SO_4 \rightarrow TiOSO_4 + FeSO_4 + H_2O$$

- FeSO₄ precipitated by chilling
- TiO₂ precipitate by heating

$$TiOSO_4 + H_2O \rightarrow TiO(OH)_2 + H_2SO_4$$

- Issues: waste
 - FeSO₄.7H₂O
 - waste H₂SO₄ neutralised to CaSO₄
- Two feeds
 - Ilmenite (49-54% TiO₂)
 - Ti slag (76-81% TiO₂)
- Ti Slag electric smelting,
 - rock ilmenites in Canada and Norway
 - High MgO contents (>3%) unacceptable for chloride pigment

What makes TiO₂ Slag soluble?



- MgO = solubility
- Slag is predominantly M₃O₅ (pseudobrookite)

MgO is particularly effective at stabilising this phase

Some of the more highly reduced rutiles are also soluble:

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Ti_4O_7 2TiO_2.Ti_2O_3 Ti_5O_9 3TiO_2.Ti_2O_3 - Magnelli phases Ti_6O_{11} 4TiO_2.Ti_2O_3
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Challenge



- Becher SR acid soluble?
- CSIRO and Iluka since the 1970's
 - behaviour of titanium minerals in reducing environments
 - Ian Grey et al at CSIRO over the last 40 years
- Ferrous pseudobrookite (FeO.2TiO₂) easy to make
 - max achievable grade is 69% TiO₂
 - too much Fe in the mineral.
- Ferrous pseudobrookite further reduced
 - TiO₂ → rutile and reduced rutiles = insoluble
- Trace elements (Mg, Mn)

STATE OF THE STREET

stabilises pseudobrookite

Stability Regions



CSIRO O₂ fugacity/T diagram

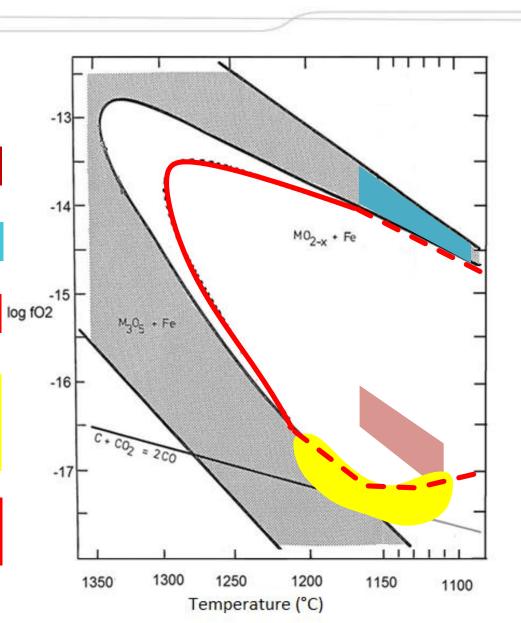
Typical operating region for SR Kiln

Low TiO₂ ferrous pseudobrookite

Impact of trace elements on M₃O₅

Pseudobrookite & reduced rutiles – high TiO₂ grade in product >90% solubility in H₂SO₄

Impact of trace elements on M₃O₅ <1200°C postulate from current work



So how?



Challenge is to operate the kiln in this preferred region

AND

- <1200°C (upper limit for refractory integrity/life)
- 1980's focussed on
 - additives Mg
 - 1200°C temperatures
- 2010's work
 - lower temperatures and
 - ilmenite with the Mg is already present in the mineral.



Reaction Pathways

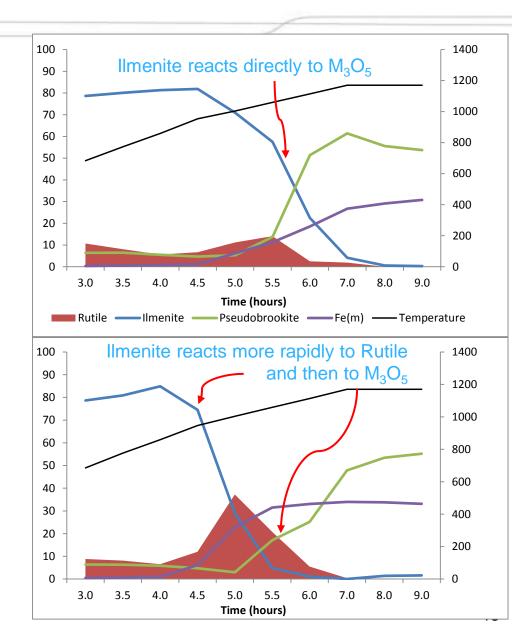


- Match high temperature metallurgy to hydrometallurgical behaviour of the product
- Starting material influences the final outcome e.g.
 - $FeO.TiO_2 \rightarrow FeO.2TiO_2 + Fe(m) \rightarrow 2TiO_2 + Fe(m)$
 - FeO.TiO₂ \rightarrow TiO₂ + Fe(m) \rightarrow Ti₃O₅ +Fe(m)
 - $Fe_2O_3.3TiO_2 \rightarrow 2FeO.TiO_2 + TiO_2 \rightarrow 2TiO_2 + 2Fe(m)$
- Same final mineralogy composition exhibit different solubility
 - a consequence of which mineral phases were present part way through the reaction sequence

Reaction pathway - coal



- Coal can impact reaction pathway.
- Normal coal
 - ilmenite directly to
 Pseudobrookite and Fe(m)
- High reductive coal
 - ilmenite reacts more quickly to rutile and Fe(m)
 - further reduction forms
 Pseudobrookite
- Increasing reactivity changes the reaction pathway



M₃O₅ Crystal Form



- Monoclinic Orthorhombic forms of Pseudobrookite
 - differences in solubility
 - feducing ilmenites with low levels of MgO.
 - this has been previously reported by Ian Grey in AI, Fe and Mg systems:
 - MgTi₂O₅-Ti₃O₅ orthorhombic to monoclinic below Mg_{0.28}Ti_{2.72}O₅
 - FeTi₂O₅-Ti₃O₅ orthorhombic to monoclinic below Fe_{0.35}Ti_{2.65}O₅
 - Al₂Ti₂O₅-Ti₃O₅ orthorhombic to monoclinic below Al_{0.45}Ti_{2.55}O₅
 - this may explain differences in solubility but still to be confirmed

State of Development



- Requirements demonstrated in the laboratory
- Demonstrated on pilot kiln + reactive coal
- Trials on 200kt/y commercial kiln planned for end of Q1 2016
- Continued laboratory test work to understand the mechanisms and the impact of the ilmenite mineralogy

Learnings



- Mineralogy is far more complex than is apparent
- Mineralogy of the final product is dependent on
 - starting mineral composition
 - reaction pathway which is itself influenced by the reduction reaction kinetics.
- Expect to be able to achieve the desired mineralogy at temperatures acceptable in the commercial kiln



